

## Analysis and Optimization of Carbon Dioxide Emission Mitigation Options in the Cement Industry

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**Abstract:** The cement industry is responsible for approximately 5% of global anthropogenic carbon dioxide emissions emitting nearly 900 kg of CO<sub>2</sub> for every 1000 kg of cement produced. Effective control strategies to mitigate these emissions are discussed and a mathematical programming model able to suggest the best cost effective strategy is outlined. Control costs consisting of operating and investment costs along with the efficiency of control options are taken into account in the model. A representative case study from the cement industry was considered in order to illustrate the use of the model in giving optimal control strategies. Efficiency improvement measures were found to be effective options for reduction targets up to 10 %. The model suggested that fuel switching and carbon capture must be considered at reduction targets higher than 10%. The cost of cement production was shown to increase dramatically with an increase in reduction target.

**Key words:** Cement industry, CO<sub>2</sub> emissions, CO<sub>2</sub> capture, process optimization

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### INTRODUCTION

The rapid deterioration of the global environment forces governments around the globe to increasingly take into consideration environmental issues. One of the most important and debated issues is the enhanced greenhouse effect due to greenhouse gases (GHG) emissions. The burning of fossil fuels releases more than six billion tonnes of carbon dioxide (CO<sub>2</sub>) into the atmosphere each year <sup>[1]</sup>. The cement industry is among the industries that release the most CO<sub>2</sub> to the atmosphere. Concrete is the world's most important construction material, and for each tonne of Portland cement (an essential component of concrete) produced, approximately one tonne of CO<sub>2</sub> is emitted to the atmosphere <sup>[2]</sup>. The cement industry generates approximately 5% of the global anthropogenic CO<sub>2</sub> emissions <sup>[3]</sup>. This is mostly due to combustion at the manufacturing operations, transportation, and combustion of fossil fuel required to produce the electricity consumed by the cement industry. Environmental policies related to CO<sub>2</sub> emissions can potentially affect greatly the cement industry. Today, there are some economically acceptable alternatives for manufacturing an environmentally-friendly Portland cement, e.g. substitute materials and alternative fuels. Whatever alternatives are implemented, they must be

pragmatic. The possibility of making a profit with CO<sub>2</sub> emissions is also a parameter that may impact the competitiveness of the cement industry.

### CEMENT FABRICATION PROCESS

Portland cement manufacturing requires a precise mix of raw materials. This mix is commonly called the raw mix and mainly consists of two main natural raw materials: limestone (calcium carbonate-CaCO<sub>3</sub>) and argillaceous materials. The cement industry must therefore start by quarrying limestone and clay. The main objective of raw material control is to produce a Kiln feed that will allow the production of a quality cement clinker, while conserving as much energy as possible. The cement clinker (clinker) requires a defined proportion of the elements calcium, silicon, aluminum, and iron; all these raw materials together with the fuel ash must combine and form the typical clinker composition. Figure 1 shows the process flow diagram of a typical cement plant <sup>[1]</sup>.

The raw material mix is grounded up before being sent to the process stage. The grinding process can be performed using either ball mills or vertical roller mills. During this stage, part of the excess heat from the Kiln is used to dry the raw mix. In order to reduce the natural chemical variation in the various raw material

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sources it is necessary to blend and homogenize the raw material efficiently. The main objective of this step is to minimize impacts on the efficiency of the Kiln.

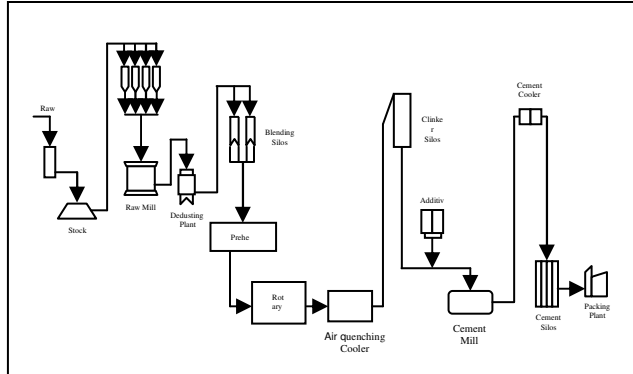


Fig.1: Process diagram of a typical cement plant

The raw material burning or clinkering step takes place in the Preheater Tower and in the Kiln. The Preheater Tower is composed of a series of countercurrent flow cyclones that transfer heat from the Kiln to the raw materials. Some of the newest Preheater Towers have a section which contains a fuel combustion chamber, called precalciner. In this stage, calcination of the raw materials will start and CO<sub>2</sub> will be formed. The Kiln is the main piece of equipment in the cement plant and “are the world’s largest piece of moving industrial process equipment and one of the hottest” [4]. The Kiln is a long, horizontal, rotating, cylindrical pipe that is at least 60 m long and can be up to 200 m long and with diameters ranging from 3 to 9 m. Its internal surface is covered with refractory bricks.

The blended raw materials are fed in to the upper end of the Preheater Tower going all the way through the end of the rotary Kiln. The Kiln slowly rotates, approximately one to four revolutions per minute, and the raw material tumbles through increasingly hotter zones. The flame at one end of the Kiln can be fuelled by powdered materials such as coal, petroleum coke, or by natural gas, oil, and recycled materials. The heat will start a series of chemical reactions and the raw material becomes molten, and fuses together into modules, called clinker, which are the final product from the Kiln. The clinker is discharged red-hot from the end of the Kiln and conducted through different types of coolers to partially recover the thermal energy and lower the clinker handling temperature. The clinker coming out of the Kiln is approximately at 1500°C. It is cooled in an air-cooled cooler. Ambient air is blown into the cooler to exchange heat between the hot clinker and the ambient air. After cooling the

clinker temperature drops to approximately 170°C. The final step to produce cement is the cement grinding, where the clinker is ground together with additives in a cement mill. The cement mill is a horizontal metallic cylinder containing metallic balls. As it rotates the crushing action of the balls grinds and mixes the clinker and additives, forming the final product.

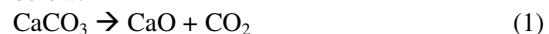
The above description illustrates clearly the energy intensity of the different steps involved in the cement industry and the corresponding CO<sub>2</sub> implications. Several studies have been conducted to reduce CO<sub>2</sub> emissions from the cement industry. Sheinbaum *et al.* [5] considered CO<sub>2</sub> abatement costs through efficiency improvement in Mexico. Hendriks *et al.* [6] shows that a wide range of options exists to reduce CO<sub>2</sub> emissions from a cement plant and provided cost data. Das and Kandpal [7] made an attempt to estimate CO<sub>2</sub> emissions from the cement industry in India. The impact of variations in product mixes and technology on CO<sub>2</sub> emissions were also analyzed. Martin *et al.* [8] presented energy efficiency and CO<sub>2</sub> emission reduction opportunities in the U.S. cement industry. Carbon capture and storage (CCS) can also represent a promising option to reduce significantly CO<sub>2</sub> emissions [1].

In this article, after identifying the various sources of CO<sub>2</sub> in a cement plant and after introducing some possible mitigation measures, a mathematical programming model that will determines the optimal CO<sub>2</sub> mitigation strategy with the least cost is presented. The objective of the model is to minimize the total control cost consisting of operating costs and investment costs. The model takes into account the sources of CO<sub>2</sub> emissions, cost, and efficiency of control options. The model is then illustrated on a case study.

## CO<sub>2</sub> EMISSIONS IN CEMENT INDUSTRY

The main sources of carbon dioxide in cement manufacturing are combustion of fossil fuel and limestone calcinations. The most common fuels are coal, petroleum coke, fuel oil and natural gas. Currently, the cement industry in North America and Europe base its fuel choice on three basic factors: cost, product quality, and environmental impact. The fuel that best fills these three basic requirements will be the preferred choice. It is important to note that factors such as the cost of a new firing system, the amount of storage, and local fuel availability also play a key role in the decision process.

During the clinker process, limestone will suffer calcination and CO<sub>2</sub> will be formed. The limestone chemical reaction can be expressed by the equation below:



The percentage of calcium oxide (CaO) in clinker is usually between 64 and 67 per cent. The balance is comprised of iron oxides, silicon oxides and aluminum oxides. The amount of CO<sub>2</sub> generated by the process varies based on the specific loss of the raw materials (limestone) on ignition. An example of mass balance for production of one tonne of cement is shown in Figure 2<sup>[9]</sup>.

There are other sources for CO<sub>2</sub> emissions in a cement plant, such as electricity and mobile equipments. These represent, however, a small contribution to the total CO<sub>2</sub> generated by the cement manufacturing. Approximately, half of the CO<sub>2</sub> emitted by the cement industry originates from the fuel and half from the calcinations (chemical reactions) that will convert raw materials into clinker<sup>[11]</sup>.

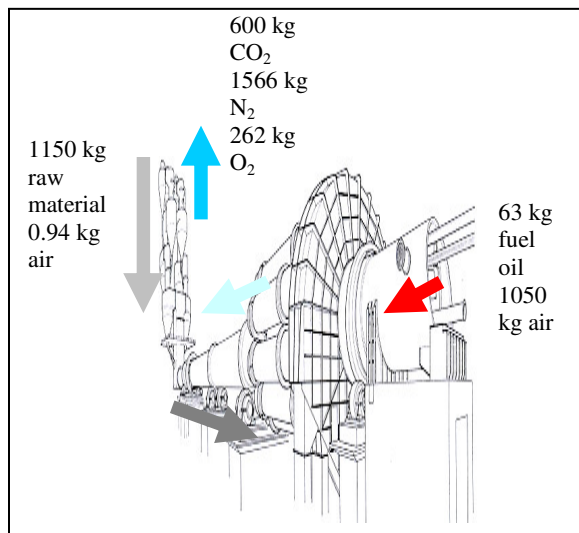


Fig. 2: Typical cement plant mass balance

### CO<sub>2</sub> MITIGATION OPTIONS

GHG mitigation has now become an important factor in creating a sustainable cement industry. Although regulated locally by different countries, the top 10 cement producers have their plants spread around the globe, and as part of a sustainability strategy, the cement industry is forced to reduce emissions. GHG mitigation has to overcome commercial and economical barriers. During the last 20 years environmental matters have had more influence in different global agreements; however, since solutions could result in a reduction in the profit margin of certain multinational corporations or adversely impact the economy of industrialized countries, the only possible solution is one that will offer environmental gains and strong business opportunities. In order to

achieve CO<sub>2</sub> mitigation targets while promoting the sustainability of the cement industry, below is a list of options that can impact on CO<sub>2</sub> emissions.

**Maintenance:** One of the most important parts of a maintenance system is preventive maintenance. Preventive maintenance can increase plant efficiency and reduce the cost of corrective maintenance. One example of results delivered by a successful maintenance system is energy savings. Actions such as false air survey and control of the leaking point can significantly increase the kiln thermo efficiency. It is estimated that a simple air leak at the kiln hood can contribute to a 46 kJ/kg of clinker increase on the kiln thermal consumption<sup>[9]</sup>.

Other strategies to reduce energy consumption include the gradual substitution of old motors by high-efficiency motors and the implementation of an integrated management system where the daily process routine contributes directly to increased maintenance effectiveness. The feeders and scales performance are examples of equipment that have direct influence on the kiln feed quality. A developed maintenance plan will support the kiln feed quality reducing the deviation on the material proportions which directly affect the fuel consumption. In general, a good maintenance program will contribute to an increase in the plant utilization ratio reducing the numbers of start-up and kiln preheats during the year<sup>[10]</sup>. Although not easily quantified, it is clear that a well structured maintenance program can highly contribute to emission reduction and plant performance improvement.

**Plant Optimization:** Plant optimization has been largely implemented in the cement industry not only as an action to reduce emissions, but also to promote higher kiln productivity and runtime. It is common knowledge in cement plants that many minor problems such as kiln seal leaks, cooler inefficiency, fuel atomization or fineness can compromise and impact plant performance. These problems alone can lead to thermal waste of up to six per cent. An optimization strategy should minimize fuel consumption and maximize clinker production correcting the clinker quality as required. The main idea is to make the process more consistent and reliable. For example, the operator might increase fan speed or reduce fuel injection based on the tower oxygen levels. It is estimated that such strategy can reduce heat consumption by three to five per cent and improve refractory life by 30 to 50 per cent<sup>[11]</sup>.

**Alternative Fuel and Pyroprocessing Improvements:** The main opportunities for improvements and reduction

of emissions associated with the cement industry are in the pyroprocess. As discussed previously, a large part of energy consumption, and consequently emission generation, takes place during the burning process. It is estimated that the average pyroprocess efficiency in the U.S. is about 34 per cent. Opportunities for improvement can be found mainly in process upgrades such as replacing wet systems and upgrading preheaters and precalciners. It is important to recognize that new burner designs and fuel systems can also play a considerable part in reducing emissions. New burners and fuel systems can contribute to reduced emissions by improving a cement plants' flexibility to burn alternative fuels, and replacing high fossil carbon fuels with low fossil carbon fuels. An example of fuel substitution is the use of natural gas instead of coal. Some other types of alternative fuels include:

- Gaseous: refinery gases and landfill gas;
- Liquid: mineral oils, distillation residues, hydraulic oil; and,
- Solid: sewage sludge, plastic, tires, petroleum coke and tar.

Other impacts of alternative fuel on the plant operation are the refractory utilization rate and preheater tower pressure loss<sup>[12]</sup>. The organic portion will burn and generate energy required for the process. The mineral part will be integrated into the process and will contribute as raw material. Fly-ash is a typical example of alternative raw material that will contribute not only as a raw material but also as an energy source.

**Replacement of Fossil Fuel by Waste-Derived Fuel (WDF):** It is estimated that the use of waste-derived fuel (WDF) will increase by one per cent worldwide per year. The alternative implemented by some cement plants is to use approximately one per cent of WDF to replace fossil fuel<sup>[13]</sup>. It is important to note that this mitigation is indirect, because if these waste products had not been burned in cement kilns, they would have been incinerated or sent to a landfill, generating further CO<sub>2</sub> emissions together with the CO<sub>2</sub> generated by the fossil fuel that was not replaced. This alternative has a potential to add great environmental value by solving the serious problem of waste disposal. Unfortunately, fossil fuel substitution by WDF is not an alternative supported by the general public. The public perception is that it would convert the cement kiln into a simple incinerator. This perception from the public pressures the local authorities to not consider this as a reasonable alternative to reduce fossil fuel consumption.

**Raw Meal Burnability:** The contribution of the raw materials burnability is difficult to measure. In general cement plants have targets for production improvement and profit margin when this alternative is considered. Raw materials fineness, composition and chemical module are the main improvements that must be made to achieve a constant raw material burnability. Such improvements could directly impact the amount of fuel used daily by the kiln. These improvements would also extend the refractory life cycle and reduce power consumption<sup>[14]</sup>.

**Use of By-products:** This alternative can provide a practical solution to the usage of huge amounts of by-products generated, such as fly ash from power plants. In some cases like fly-ash, the by-product can contribute to improve concrete durability. This alternative needs to be studied locally to determine the availability and cost. European countries have been using by-products in high amounts. In general, it is important to note that cement standards need to be reviewed to accommodate the use of by-products as alternatives in the process of reducing GHG emissions<sup>[15]</sup>.

**Replacing Raw Material Limestone by Slag:** Blast furnace slag is a non-metallic by-product from the iron production process. It is comprised of silicates, aluminosilicates, and calcium-alumina-silicates. By replacing raw material limestone with slag it is possible not only to prevent CO<sub>2</sub> emissions due to limestone decomposition, but also to improve raw material burnability. Blast furnace slag is not a new supplementary cementitious material; it has been used by the cement industry as a component blended in cement or as aggregate material in the concrete mixture for the past ten years. Blast furnace slag incorporation in Portland cement is specified by AASHTO M302<sup>[16]</sup>. Although blast slag has great use in the cement industry, its use cannot be generalized worldwide, since factors such as the cost of slag and transportation are prohibitive. It is important to observe that only 25 per cent of the energy used to manufacture Portland cement is required. The use of slag has important ecological and economical benefits. For example, the use of slag in Europe has contributed significantly to the efforts to meet the Kyoto targets, and has reduced the energy and raw materials necessary in the cement process<sup>[17]</sup>.

**Electrical Energy Savings:** Electrical energy is used in the cement plant to drive fans, rotate the kiln and to

move materials. In general, the power used in the kiln corresponds to 40 to 50 kWh/tonne clinker. Power savings from the use of high efficiency motors will vary from plant to plant and from case to case. Most of the motor substitution is done during the replacement period when the motor life is nearly done. Another energy consumption point in the cement process is the adjustable speed drivers. Drivers are, in most cases, the largest power consumers in the cement process. Adjustable drivers can produce savings from 7 to 60 per cent <sup>[4]</sup>. These savings will be based on the application and the load applied to the motor and the application in the process.

**New Preheater Tower:** The preheater tower is a vital part of the process. A new preheater tower with low pressure drop cyclones will reduce the power consumption of the kiln fan system. It is possible to achieve a reduction of 0.6 to 1.1 kWh/t depending on the fan efficiency. A new installation can be expensive. In addition, installation and modification are site-specific, which makes it difficult to point out a general return on the investment. A new cyclone system can increase the overall dust transport cost <sup>[18]</sup>. This indicates that this solution is recommended for dry preheater and precalciner kilns older than 15 years of age.

**Kiln Burner:** Burner technology has improved quickly. A number of different burners have improved flame control and optimized fuel usage. One of the main objectives of the new burner technology is to create a more stable flame independent of the fuel type. Flame stability is one of the most important factors in maintaining a stable kiln operation and maximizing combustion effectiveness.

**CO<sub>2</sub> Capture and Disposal:** Different methods for the capture and disposal of CO<sub>2</sub> at the point of combustion have been researched and developed <sup>[1]</sup>. Examples of possibilities are: chemical stripping, membrane system, cryogenic separation and physical absorption. The implementation cost of each one of these possibilities is highly uncertain; costs are directly related to technical performance, economic growth and fuel type. Moreover, the disposal solutions available today present a great level of doubt regarding the technical feasibility for a full-scale implementation.

The CO<sub>2</sub> concentration in a cement plant is higher than in a power generation process. Studies have shown that the cement production process has a high quantity of low quality heat. This extra heat could be used in the CO<sub>2</sub> capture process <sup>[19]</sup>. In general, the average cost to

capture one tonne of CO<sub>2</sub> is estimated to be around USD 50 <sup>[1]</sup>.

Chemical scrubbing is considered to be the most mature process to capture CO<sub>2</sub>. The chemical stripping method is based on Henry's Law where the absorption depends on the temperature and pressure of the system. Chemical absorption is mainly applicable for a system where the exhaust gases present low concentration of CO<sub>2</sub> and the system pressure is close to atmospheric pressure. The main steps of the stripping method are absorption of CO<sub>2</sub> by chemical solvents and recovery of CO<sub>2</sub> from chemical solvents by using low-grade heat (usually extracted from power plants). One of the available technologies for removing CO<sub>2</sub> from the gas stream is chemisorption using monoethanolamine. The design and costing of CO<sub>2</sub> capture from cement plant flue gas is similar to the design and costing of capturing CO<sub>2</sub> from power plant using monoethanolamine <sup>[1]</sup>. At a typical cement plant the cost for this method was estimated to be approximately \$49-\$54 per tonne of CO<sub>2</sub> captured <sup>[1]</sup>.

Physical absorption is another option for capturing CO<sub>2</sub> and has its main application with low concentration gases and vapors that are retained in a surface of porous solid materials. CO<sub>2</sub> is held on the surface of the porous material by (non-chemical) surface forces. The solid adsorbent material is regenerated using heat and the CO<sub>2</sub> capture is complete <sup>[20]</sup>.

Membrane systems are based on different physical and chemical interactions between the gas stream and the membrane material. Carbon dioxide capture by a membrane system is currently not considered as a common approach. The main obstacle for this technology is the necessity of multiple stages or cycles, which directly increases energy consumption and consequently, cost.

the cryogenic fraction method is based on the compression of the gas stream and subsequently, the gas temperature is reduced where the separation is possible by distillation. This method is mainly recommended in cases of high CO<sub>2</sub> concentration (more than 90 per cent) and therefore is not suitable for the cement industry.

As for CO<sub>2</sub> disposal, the options are: discharge into natural gas reservoirs or aquifers, discharge deep into the ocean or reuse the CO<sub>2</sub> in useful organic compounds. Reviewing all the solutions available today, the ocean scenario has the highest capacity to store CO<sub>2</sub>, and absorbs the CO<sub>2</sub> quantities generated by the actual necessity of reduction <sup>[21]</sup>. It is expected that in the next few years, CO<sub>2</sub> underground storage will be

a technical and economical option for CO<sub>2</sub> disposal, especially in the case of enhanced oil recovery and eventually coal bed methane recovery.

### MATHEMATICAL MODEL

The above section illustrates clearly that there is a wide range of options that can be used to reduce CO<sub>2</sub> emissions in the cement industry. These include:

- Improvement of the energy efficiency of the process
- Shifting to a more energy efficient process (e.g. from (semi) wet to dry process)
- Replacing high carbon fuels by low carbon fuels
- Removal of CO<sub>2</sub> from the flue gases such as by absorption (MEA process)

In order to help decision makers to adapt an appropriate CO<sub>2</sub> reduction strategy, an optimization model for the cement industry is presented in this section. The mathematical model consists of an objective function to be minimized and equality and inequality constraints. The objective of the model is to find the best strategy or mix of strategies to reduce CO<sub>2</sub> up to a certain target with minimum overall cost for cement production while meeting the demand.

The objective function to be minimized can be written as:

$$Z(\$/yr) = \sum_r C_r R_r + \sum_i \sum_f C_{if} P_{if} + \sum_i \sum_f R_{if} X_{if} + \sum_i \sum_e C_{ie} Y_{ie} + \sum_i \sum_c C_{ic} Z_{ic} \quad (2)$$

Where:

Z : annualized capital and operating cost of the cement plant (\$/yr)

C<sub>r</sub> : cost of purchasing raw material r (\$/tonne)

R<sub>r</sub> : purchased amount of raw material r (tonne/yr)

C<sub>if</sub> : operating cost for a unit i with fuel f (\$/tonne)

P<sub>if</sub> : amount produced from unit i using fuel f (tonne/yr)

R<sub>if</sub> : annualized retrofit cost for switching unit i to run with another fuel f (\$/yr)

X<sub>if</sub> : binary variable representing switching or not.

C<sub>ie</sub> : annualized cost of applying efficiency improvement technology (e) on unit i (\$/yr)

Y<sub>ie</sub> : binary variable representing applying efficiency improvement technology (e) or not.

C<sub>ic</sub> : annualized cost of applying CO<sub>2</sub> capture technology (c) on unit i (\$/yr)

Z<sub>ic</sub> : binary variable representing applying CO<sub>2</sub> capture technology (c) or not.

The first term in the objective function represents the cost associated with purchasing the raw material. The second term takes into account the operating cost for different units. The cost of switching to less carbon content fuel is shown in the third term. The fourth term represents the cost associated with applying efficiency improvement technologies. The remaining term adds the cost that results from applying CO<sub>2</sub> capture technology. A binary variable is defined for each CO<sub>2</sub> mitigation option under study.

**Constraints:** The constraints for demand satisfaction, fuel selection and CO<sub>2</sub> emissions reduction are described as follows:

a) Demand satisfaction

This constraint simply says that the total cement produced should be greater than or equal to the demand.

$$\sum_i \sum_f P_{if} \geq demand \quad (3)$$

b) Fuel selection

Each unit i has to run with only one fuel f. For this reason, a binary variable is introduced to represent the type of fuel used in a given unit.

$$\sum_f X_{if} = 1 \quad \forall i \quad (4)$$

c) Emission constraint

The CO<sub>2</sub> emitted from all units must satisfy a CO<sub>2</sub> reduction target. Different technologies, e, to improve the efficiency are implemented in the mathematical model. It is assumed that the effect of these technologies is additive. The emission is also affected by applying CO<sub>2</sub> capture technology.

$$\sum_i \sum_f CO_{2if} \left( 1 - \sum_e e_{ie} Y_{ie} \right) \left( 1 - \sum_c \epsilon_{ic} Z_{ic} \right) P_{if} \leq (1 - \%CO_2) CO_2 \quad (5)$$

Where:

CO<sub>2if</sub> : CO<sub>2</sub> emissions from unit i using fuel f (tonne per tonne cement produced)

e<sub>ie</sub> : percent gain in efficiency associated with applying technology e on unit i

Y<sub>ie</sub> : binary variable for applying efficiency improvement technology e or not

ε<sub>ic</sub> : percent CO<sub>2</sub> capture

Z<sub>ic</sub> : binary variable for applying CO<sub>2</sub> capture technology c or not

% CO<sub>2</sub>: reduction target

CO<sub>2</sub> : Current CO<sub>2</sub> emissions (tonne/yr)

d) Selection of CO<sub>2</sub> capture process to be installed  
This constraint let the model select only one capture process for each unit *i*

$$\sum_c Y_{ic} \leq 1 \quad \forall i \quad (6)$$

e) Non-negativity constraints

The amount produced must be greater than zero

$$P_{if} \geq 0 \quad \forall i \quad (7)$$

The developed model is illustrated in the following case study.

### Case Study

The problem of reducing CO<sub>2</sub> emissions from combustion sources within a cement plant is considered with three different mitigation options. The first option is the application of efficiency improvement technologies to reduce CO<sub>2</sub> emissions. Table 1 shows the different technologies considered in this study, along with their corresponding reduction in CO<sub>2</sub> emissions. The second option for reducing CO<sub>2</sub> emissions is the switching of fuel to a less carbon content fuel (e.g. switch from coal to natural gas). The third option is the application of CO<sub>2</sub> capture technologies.

An existing cement plant [22] with the following data was studied and the aim is to minimize the cost of cement production while reducing CO<sub>2</sub> emissions by a fixed target.

Cement production: 712,600 tonne/yr

Current total CO<sub>2</sub> emissions: 553,800 tonne CO<sub>2</sub>/yr

Current total annualized cost: 25 x 10<sup>6</sup> \$/yr

Three CO<sub>2</sub> mitigation options will be considered and these are:

- Applying efficiency improvement technologies to reduce CO<sub>2</sub> emissions shown in Table 1.
- Switching to less carbon content fuel such as from coal to natural gas
- Applying “end of pipe” CO<sub>2</sub> capture technologies. The chemical absorption (MEA) process is the only considered option in this study with a cost of 50 \$/tonne CO<sub>2</sub> captured.

The model is first formulated as a mixed integer nonlinear model (MINLP). This model was then linearized using an exact linearization scheme similar to what we have employed in our previous work on

carbon dioxide mitigation in the power industry [23]. The resulting linearized model (mixed integer linear program or MILP) was coded in GAMS (General Algebraic Modeling System).

Table 1: Technologies for efficiency improvements

Technology	% CO <sub>2</sub> Reduction
High efficiency motors and drives	4
Adjustable Speed Drives	5.5
High efficiency classifiers	8.1
Efficient grinding technologies	10.5
Conversion from wet to dry process	50.0

### DISCUSSION

The CO<sub>2</sub> mitigation options discussed earlier were incorporated into the model to select the least cost option to reduce CO<sub>2</sub> emissions to a specified target. Different CO<sub>2</sub> reduction targets were specified. Table 2 shows the results for different CO<sub>2</sub> reduction targets. For 1% reduction target, for example, the optimization process chose to apply the technology of high efficient motors and drives. The cost of production increased by about 2%. A second improvement technology was selected by the model at a reduction target of 5%. No fuel switching was applied up to 10 % where efficiency improvement technologies can be applied with an increase of about 7% in the cost. For a 20 reduction target, fuel switching, from coal to natural gas, was selected with only one technology for efficiency improvement (installation of high efficient motors and drives). The cost increased by about 17%. Carbon capture technology was selected at reduction targets higher than 30%. For a 50% reduction target, the optimization process still chose to apply capture technology.

Table 2: Summary of results for different CO<sub>2</sub> reduction target

% CO <sub>2</sub> reduction	Cost (million \$/yr)/ (\$/tonne cement)	% Increase in cost
0	25.0 / 35.1	0
1	25.6 / 35.9	2.4
5	25.7 / 36.1	2.9
10	26.8 / 37.6	7.3
20	29.4 / 41.2	17.4
30	33.3 / 46.7	33.2
50	38.9 / 54.5	55.4

Figure 3 shows the increase in the production cost for each CO<sub>2</sub> reduction target. The line starts to sharply increase at reduction targets ranging from 20 to 50%. This is expected since this is where optimization lead to decisions that employ CO<sub>2</sub> capture options which have in general a much higher cost than other mitigation options.

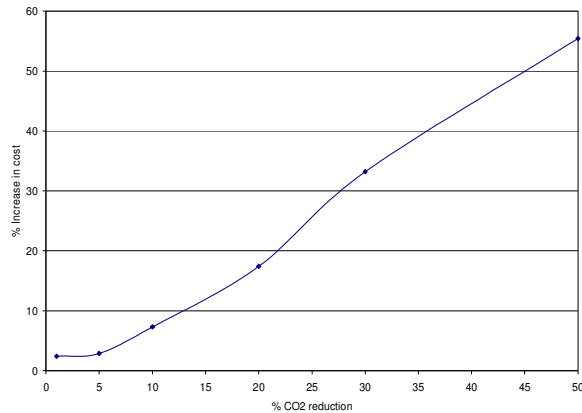


Fig. 3: Percent increase in cost for different CO<sub>2</sub> reduction targets

### CONCLUSIONS

An optimization model was developed in order to meet demand at a given CO<sub>2</sub> reduction target. Three mitigation options were considered. The model chose the best strategy or mix of strategies in order to meet a certain CO<sub>2</sub> reduction target with the least cost providing that the demand and other requirements were met. The model was formulated as a MINLP, exactly linearized, and then coded in GAMS.

It was found that the application of different efficiency improvement technologies represent good options especially at reduction targets up to 10%. Beyond this reduction target, fuel switching should be applied to achieve a reduction target such as 20%. At reduction targets higher than 20%, carbon capture technologies should be applied and efficiency improvement technologies are no more a good mitigation option. The cost of production increased dramatically when the reduction target is beyond 20%. This is because carbon capture technologies were selected at these ranges and since these were the most expensive mitigation options. The cost per tonne Portland cement produced increased from 35.1 \$/tonne to about 55 \$/tonne which is about 20 \$ increase for each tonne produced.

### REFERENCES

1. Nazmul, S.M., E. Croiset, and P.L. Douglas, 2006. Techno-Economic study of CO<sub>2</sub> capture from an existing cement plant using MEA scrubbing. *International Journal of Green Energy*, 3: 1-24.
2. Natural Resources Canada Climate Change 2006, 'Cement and Concrete', available: <http://climatechange.nrcan.gc.ca> (accessed: 15 March 2007).
3. IPCC. 2001. *Climate Change 2001: the scientific basis*. Intergovernmental Panel on Climate Change, Cambridge University Press, Cambridge, UK.
4. Choate, T.W., 2003. *Energy and Emission Reduction Opportunities for the Cement Industry*, Industrial Technologies Program, U.S Department of Energy, Energy Efficiency and Renewable Energy, 14: 24-29.
5. Sheinbaum, C., I. Jauregui and L. Rodriguez, 1998. Carbon dioxide emission reduction scenarios in Mexico for year 2005. *Mitigation and Adoption Strategies for Global Change*, 2: 359-372.
6. Hendriks, C., E. Worrel, D. Dejager, K. Blok, and P. Riemer, 2004. Emission reduction of greenhouse gases from the cement industry. *Greenhouse gas control technologies conference*, 1-11.
7. Das, A. and T.C. Kandpal, 1997. Energy environment implications of cement manufacturing in India. *Int. J. Energy Research*, 21: 299-308.
8. Martin, N., E. Worrel, and L. Price, 1999. *Energy efficiency and carbon dioxide emissions reduction opportunities in the U.S. Cement Industry*. Environmental energy technologies division report.
9. IEA Greenhouse Gas R&D, 1999. *The reduction of greenhouse gas emissions from the cement industry*. Report Number PH3/7, 25-49.
10. Saxena, J.P., 1995. Productivity improvements through reduction in Kiln downtime. *World Cement*, 26 (3), 64-68.
11. Votorantim 1994. *Sistema especialista automatiza 25 linhas de cimento*, Minérios/Minerales Magazine, São Paulo, 196, 28-29.
12. Grosse-Daldrup, H. and B. Scheubel, 1996. *Alternative fuels and their impact on the refractory linings*. Refratechnik Report, No. 45.
13. Kihara, Y., 1999. *Co-processamento de resíduos em fornos de cimento: tendências*. Proceedings of II Seminário Desenvolvimento Sustentável e a Reciclagem na Construção Civil, Organised by Comitê Técnico do IBRACON CT-206-Meio Ambiente, São Paulo, Brazil, 35-43.



14. Gouda, G.R., 1977. Cement raw materials and their effect on fuel consumption. *Rock Products*, Chicago, 80 (10), 60-64.
15. Damtoft, J.S., 1998. Use of fly ash and other waste materials as raw feed and energy source in the Danish cement industry. *Proceedings of Three-Day CANMET/ACI International Symposium on Sustainable Development of Cement and Concrete Industry*, Ottawa, Canada, CANMET/ACI, 95-105.
16. Collins, R. J. and S.K. Ciesielski, 1994. Recycling and Use of Waste Materials and By-Products in Highway Construction. *National Cooperative Highway Research Program Synthesis of Highway Practice 199*, Transportation Research Board, Washington, DC, 1994.
17. Ehrenberg, A. 2002. CO<sub>2</sub> emissions and energy demand of granulated blast furnace slag. *Proceedings of the 3<sup>rd</sup> European Slag Conference*, EUROSLAG publication, 2, 151-166.
18. Jepsen, O.L. and K.P. Christensen, 1998. Improving fuel consumption and emissions by means of modern cooler, cyclone and calciner technology. *Proceedings of WABE International Symposium on Cement and Concrete*, Montreal, Canada, 5-15.
19. Thambimuthu, K.V., 2002. CO<sub>2</sub> Capture and Reuse. *CANMET Energy Technology Centre, Natural Resources Canada IEA Greenhouse Gas R&D Programme Cheltenham*, United Kingdom.
20. Cooper C. D. and F.C. Alley, 2002. *Air Pollution Control - A Design Approach*.. Waveland Press, Inc., Illinois.
21. Eckaus, R.S., H.D. Jacoby, A. D. Elterman, W.C. Leug W.C., and Z. Yang, 1997. *Economical assessment of CO<sub>2</sub> capture and disposal*. Joint Program on the Science and Policy of Global Change, Massachusetts Institute of Technology, Cambridge, MA.
22. Elkamel, A., A. Elgibaly, and W. Bouhamra, 1998. Optimal air pollution control strategies: the retrofitting problem. *Advances in environmental research*, 2 (3): 375-389.
23. Ba-Shammakh, M, A. Elkamel, P.L. Douglas, and E. Croiset, 2007. A mixed-integer nonlinear programming model for CO<sub>2</sub> emission reduction in the power generation sector. *International Journal of Environment and Pollution*, 29 (1/2/3): 254-273.